Low Mach number models: some advantages for numerical simulations of weakly compressible flows with high heat transfers

Bérénice GREC¹

in collaboration with S. Dellacherie, G. Faccanoni et Y. Penel

¹MAP5 – Université Paris Descartes, France

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MEMBRE DE

USING CENTRAL Sorbonne Paris Cité

Outline of the talk



- 2 Equation of state and taking into account phase transition
 - 3 Theoretical results on the LMNC model
 - 4 Numerical approach and results
- 5 Conclusion and prospects

Pressurized Water Reactor (PWR)



Core of a Pressurized Water Reactor (PWR)



Low Mach number: which model for which regime?

Nominal regime

- Entrance velocity: $|\boldsymbol{u}| \simeq 5 \,\mathrm{m}\cdot\mathrm{s}^{-1}$
- ▶ Sound speed at $p_0 = 155$ bar and T = 300 °C: $c_\ell^* \simeq 1.0 \times 10^3 \,\mathrm{m \cdot s^{-1}}$
- Mach number (measures the compressibility of the flow):

$$\mathrm{Ma} = \frac{|\boldsymbol{u}|}{c_{\ell}^*} \simeq 5 \times 10^{-3} \ll 1$$

Choice of the model:

- Compressible Navier-Stokes/Euler?
- Incompressible?
- Adapted model for the low Mach regime?

Negligible acoustic phenomena (no shock waves) BUT high heat transfers: $\operatorname{div} \boldsymbol{u} \neq 0$ \Rightarrow Asymptotic model at low Mach number

 \Rightarrow Asymptotic model at low Mach number

From compressible Navier-Stokes to LMNC model

Compressible Navier-Stokes system

$$\begin{cases} \partial_t \rho + \operatorname{div}(\rho \boldsymbol{u}) = 0, \\ \partial_t(\rho \boldsymbol{h}) + \operatorname{div}(\rho \boldsymbol{h} \boldsymbol{u}) = \Phi + \operatorname{div}(\lambda \nabla T) + \partial_t p + \boldsymbol{u} \cdot \nabla p + \sigma(\boldsymbol{u}) :: \sigma(\boldsymbol{u}), \\ \partial_t(\rho \boldsymbol{u}) + \operatorname{div}(\rho \boldsymbol{u} \otimes \boldsymbol{u}) - \operatorname{div} \sigma(\boldsymbol{u}) + \nabla p = \rho \boldsymbol{g}. \end{cases}$$

- Unknowns
 - $(t, \mathbf{x}) \mapsto \mathbf{u}$: velocity
 - $(t, \mathbf{x}) \mapsto h$: enthalpy
 - $(t, \mathbf{x}) \mapsto p$: pressure
 - ρ , T: density and temperature linked to h and p through the equation of state
- Data
 - $(t, \mathbf{x}) \mapsto \Phi \ge 0$: power density
 - ► g: gravity
 - λ : thermal conductivity
 - $\sigma(\mathbf{u})$ stress tensor (viscosity)

From compressible Navier-Stokes to LMNC model

Compressible Navier-Stokes system

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Boundary conditions



From compressible Navier-Stokes to LMNC model

Compressible Navier-Stokes system

$$\begin{cases} \partial_t \rho + \operatorname{div}(\rho \boldsymbol{u}) = 0, \\ \partial_t(\rho \boldsymbol{h}) + \operatorname{div}(\rho \boldsymbol{h} \boldsymbol{u}) = \Phi + \operatorname{div}(\lambda \nabla T) + \partial_t p + \boldsymbol{u} \cdot \nabla p + \mathcal{O}(\varepsilon^2), \\ \partial_t(\rho \boldsymbol{u}) + \operatorname{div}(\rho \boldsymbol{u} \otimes \boldsymbol{u}) - \operatorname{div} \sigma(\boldsymbol{u}) + \frac{1}{\varepsilon^2} \nabla p = \rho \boldsymbol{g}. \end{cases}$$

• Dimensionless system: $Ma = \varepsilon$ and asymptotic expansion

$$p = p^{(0)} + \varepsilon p^{(1)} + \varepsilon^2 p^{(2)} + \mathcal{O}(\varepsilon^3)$$

• $\nabla p^{(0)} = \nabla p^{(1)} = 0$ with outlet boundary condition independent of t

$$\implies p(t, \mathbf{x}) = p_* + \varepsilon^2 \bar{p}(t, \mathbf{x}).$$

Pressure is decomposed into a thermodynamical constant part p_* and a dynamical part of order $\varepsilon^2 \ \overline{p}$.

Low Mach number model

LMNC Model

$$\begin{cases} \operatorname{div} \boldsymbol{u} = \frac{\beta(h, p_*)}{p_*} \Big[\Phi + \operatorname{div} \left(\Lambda(h, p_*) \nabla h \right) \Big], \\ \rho(h, p_*) \Big(\partial_t h + \boldsymbol{u} \cdot \nabla h \Big) = \Phi + \operatorname{div} \left(\Lambda(h, p_*) \nabla h \right), \\ \rho(h, p_*) \Big(\partial_t \boldsymbol{u} + (\boldsymbol{u} \cdot \nabla) \boldsymbol{u} \Big) + \nabla \bar{p} = \operatorname{div}(\sigma(\boldsymbol{u})) + \rho(h, p_*) \boldsymbol{g}. \end{cases}$$

- Compressibility coefficient $\beta(h, p_*) = -\frac{p_*}{\rho^2} \frac{\partial \rho}{\partial h}(h, p_*)$
- Equation of state: analytical or tabulated \rightsquigarrow for example, stiffened gas (SG) : $\rho(h, p_*) = \frac{\gamma}{\gamma - 1} \frac{p_* + \pi}{h - a}$
- Rewriting the thermal diffusion term

$$\lambda(h, p_*) \nabla T = \frac{\lambda(h, p_*)}{c_p(h, p_*)} \nabla h = \Lambda(h, p_*) \nabla h$$

► Stress tensor $\sigma(\boldsymbol{u}) = \mu(h, p_*) \left(\nabla \boldsymbol{u} + (\nabla \boldsymbol{u})^T \right) + \eta(h, p_*) (\operatorname{div} \boldsymbol{u}) \operatorname{Id}$

Low Mach number model

LMNC Model

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Initial and boundary conditions



Analysis of low Mach number models

- ► Applications in combustion: Majda, Klein, ...
- ► Applications in astrophysics Colella, Almgren, ...
- ► Applications in nuclear industry: Bell, Paillère, Dellacherie, ...

Theoretical studies

- ► Klainerman & Majda ('81, '82): barotropic models (some domains)
- Schochet ('94): convergence for barotropic Euler with any IC
- ► Desjardins, Grenier, Lions & Masmoudi ('99): bounded domains
- ► Danchin ('01, '05): extension to Besov spaces
- Alazard ('05): extension to general equations of state

Numerical aspects

- Klein ('95): operator splitting
- ► Guillard et al. ('99, '04, '08): asymptotic expansion in Ma in the schemes
- ► Dellacherie *et al.* ('10, '13): analysis of schemes thanks to Schochet decomposition, stability of the discrete kernels

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Diphasic equation of state

- Liquid κ = ℓ and vapor κ = g are characterized by their thermodynamical properties: (h, p_{*}) → ρ_κ
- ► In the mixture, equilibrium between liquid and vapor phases: T = T^s(p_{*}). Saturation values can be defined

$$h^s_\kappa(p_*) \stackrel{\text{def}}{=} h_\kappa(p_*, T^s(p_*)), \qquad \rho^s_\kappa(p_*) \stackrel{\text{def}}{=} \rho_\kappa(h^s_\kappa, p_*).$$

$$\rho(h, p_*) = \begin{cases} \rho_{\ell}(h, p_*), & \text{if } h \le h_{\ell}^{s}(p_*), \\ \rho_{m}(h, p_*) & \text{if } h_{\ell}^{s}(p_*) < h < h_{g}^{s}(p_*), \\ \rho_{g}(h, p_*), & \text{if } h \ge h_{g}^{s}(p_*). \end{cases}$$



Equation of state in the mixture and analytical laws

Defining α the volume fraction of vapor phase, equilibrium gives

$$\begin{cases} \rho = \alpha \rho_g^{\mathsf{s}}(p_*) + (1 - \alpha) \rho_\ell^{\mathsf{s}}(p_*) \\ \rho h = \alpha \rho_g^{\mathsf{s}}(p_*) h_g^{\mathsf{s}}(p_*) + (1 - \alpha) \rho_\ell^{\mathsf{s}}(p_*) h_\ell^{\mathsf{s}}(p_*) \end{cases}$$

for
$$h\in [h^s_\ell(p_*);h^s_g(p_*)]$$

Density in the mixture

 $ho_m(h,p_*) = rac{p_*/eta_m(p_*)}{h-q_m(p_*)}, ext{ where } eta_m ext{ and } q_m ext{ depend only on the saturation values.}$

Noble Able Stiffened Gas (NASG)

$$\frac{1}{\rho_{\kappa}}(h, p_{*}) = \frac{\gamma_{\kappa} - 1}{\gamma_{\kappa}} \frac{h - q_{\kappa}}{p_{*} + \pi_{\kappa}} + b_{\kappa}$$

We compute $\beta_{\kappa}(p_{*})$ independent of h
New expression of ρ

- $\gamma_{\kappa} > 1$ adiabatic coefficient
- π_{κ} reference pressure
- q_{κ} binding energy, b_{κ} covolume

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Equation of state in the mixture and analytical laws

Defining α the volume fraction of vapor phase, equilibrium gives

$$\begin{cases} \rho = \alpha \rho_g^s(p_*) + (1 - \alpha) \rho_\ell^s(p_*) \\ \rho h = \alpha \rho_g^s(p_*) h_g^s(p_*) + (1 - \alpha) \rho_\ell^s(p_*) h_\ell^s(p_*) \end{cases}$$

for
$$h\in [h^s_\ell(p_*);h^s_g(p_*)]$$

Density in the mixture

 $\rho_m(h, p_*) = \frac{p_*/\beta_m(p_*)}{h - q_m(p_*)},$ where β_m and q_m depend only on the saturation values.

Noble Able Stiffened Gas (NASG)

$$\frac{1}{\rho_{\kappa}}(h, p_{*}) = \frac{\gamma_{\kappa} - 1}{\gamma_{\kappa}} \frac{h - q_{\kappa}}{p_{*} + \pi_{\kappa}} + b_{\kappa}$$
We compute $\beta_{\kappa}(p_{*})$ independent of h
New expression of ρ

$$ho_\kappa(h,p_*)=rac{p_*/eta_\kappa(p_*)}{h-\hat{q}_\kappa(p_*)}, \qquad \hat{q}_\kappa(p_*)\stackrel{ ext{def}}{=} q_\kappa-rac{p_*}{eta_\kappa(p_*)}b_\kappa$$

- $\gamma_{\kappa} > 1$ adiabatic coefficient
- π_{κ} reference pressure
- q_{κ} binding energy, b_{κ} covolume

 $h_{\ell}^{s}(p_{*}) h_{\sigma}^{s}(p_{*})$

Equation of state for pure phases: tabulated data

	h_{κ}	ϱ_{κ}	T_{κ}		β_{κ}
κ	$[kJ \cdot kg^{-1}]$	$[\text{kg} \cdot \text{m}^{-3}]$	[K]		
l	978.702	842.783	500.000		X
ℓ	980.223	842.359	500.336		X
÷	:	÷	:	÷	÷
ℓ	1627.450	595.733	617.667		X
ℓ	$h_{\ell}^{s} = 1629.880$	594.379	<i>T^s</i> =617.939		×
g	$h_g^s = 2596.119$	101.930	<i>T^s</i> =617.939		X
g	2596.965	101.816	618.00		×
÷	:	:	:	÷	÷
g	3066.962	60.540	699.667		X
g	3068.184	60.473	700.000		X

Source:http://webbook.nist.gov/chemistry/fluid/

Quantities c_{κ}^* , $c_{p_{\kappa}}$, $c_{v_{\kappa}}$, λ_{κ} , μ_{κ} are also tabulated.

Equation of state for pure phases: tabulated data at p_*

New expression of the compressibility coefficient:

$$\beta = \frac{p}{\rho c^* \sqrt{T}} \sqrt{\frac{1}{c_v} - \frac{1}{c_p}}$$

 \Longrightarrow fitting of β for tabulated data for T, c_v, c_p, c^*, ρ

$$eta_\kappa(h, p_*) pprox ilde{eta}_\kappa(h) := \sum_{j=0}^{d_{eta,\kappa}} b_{\kappa,j} \left(rac{h}{10^6}
ight)^j.$$

Reconstruction of ρ

$$\frac{1}{\rho}(h,p_*) \approx \frac{1}{\tilde{\rho}(h)} := \begin{cases} \frac{1}{\tilde{\rho}_\ell}(h) := \frac{1}{\rho_\ell^s(p_*)} + \int_{h_\ell^s}^h \frac{\tilde{\beta}_\ell(h)}{p_*} dh, & \text{if } h \le h_\ell^s, \\ \frac{1}{\rho_m}(h), & \text{if } h_\ell^s < h < h_g^s, \\ \frac{1}{\tilde{\rho}_g}(h) := \frac{1}{\rho_g^s(p_*)} + \int_{h_g^s}^h \frac{\tilde{\beta}_g(h)}{p_*} dh, & \text{if } h \ge h_g^s. \end{cases}$$

Equation of state for pure phases: tabulated data at p_*

New expression of the compressibility coefficient:

$$\beta = \frac{p}{\rho c^* \sqrt{T}} \sqrt{\frac{1}{c_v} - \frac{1}{c_p}}$$

 \Longrightarrow fitting of β for tabulated data for T, $\textit{c_v},~\textit{c_p},~\textit{c}^*,~\rho$

$$eta_\kappa(h, p_*) pprox ilde{eta}_\kappa(h) := \sum_{j=0}^{d_{eta,\kappa}} b_{\kappa,j} \left(rac{h}{10^6}
ight)^j.$$

Proposition

• The relation
$$ilde{eta} = -rac{m{p}_*}{ ilde{
ho}^2}rac{\partial ilde{
ho}}{\partial h}$$
 is satisfied exactly;

 \bullet $h \mapsto \tilde{\rho}(h)$ is continuous, positive and decreasing on (h_{\min}, h_{\max}) .

Choice of the degree $d_{\beta,\kappa}$ according to desired precision

 \rightsquigarrow Even with $d_{eta,\kappa}=$ 0, better results than with analytical EOS such as (NA)SG

3

 $h/10^{6} (J \cdot K^{-1})$

500

0

1,500

(g 1,000 - H · By) - 500

0

0

0.2

0.1

0

4

2 3

 $h/10^{6} (J \cdot K^{-1})$

Comparison of the equations of state

	SG	NASG	NIST	
h_ℓ^s h_g^s	$\begin{array}{c} 1.627 \times 10^{6} \ \text{J} \cdot \text{kg}^{-1} \\ 3.004 \times 10^{6} \ \text{J} \cdot \text{kg}^{-1} \end{array}$	$\begin{array}{c} 1.596 \times 10^{6} \ \text{J} \cdot \text{kg}^{-1} \\ 2.861 \times 10^{6} \ \text{J} \cdot \text{kg}^{-1} \end{array}$	$\begin{array}{c} 1.629 \times 10^{6} \ \text{J} \cdot \text{kg}^{-1} \\ 2.596 \times 10^{6} \ \text{J} \cdot \text{kg}^{-1} \end{array}$	
ρ_{ℓ}^{s} ρ_{g}^{s}	$\begin{array}{c} 632.663kg\cdot m^{-3} \\ 52.937kg\cdot m^{-3} \end{array}$	737.539 kg \cdot m ⁻³ 55.486 kg \cdot m ⁻³	$\begin{array}{c} 594.38kg\cdot m^{-3} \\ 101.93kg\cdot m^{-3} \end{array}$	
T ^s	654.65 K	636.47 K	617.939 K	
	^j ^j ^j ^j ^j ^j ^j ^j	\$\vec{q}\$ \$\vec{q}\$ \$\vec{q}\$ \$\vec{r}\$ \$\vec{r}\$ \$\vec{r}\$	0.5 0.4 0.4 0.3 0.3 0.3 0.3 0.3 0.3 0.3 0.3	



2 3

 $h/10^{6} (J \cdot K^{-1})$

Comparison of the equations of state



Incomplete equation of state adapted to the low Mach approach where $p = p_*!$

Tabulated data when taking into account thermal diffusion

We can use (independently) the same approach to define $T(h, p_*)$ and $c_p(h, p_*)$.

Fitting $1/c_p$ from tabulated data

$$rac{1}{c_{{m
ho}_\kappa}(h,{m
ho}_*)}pprox rac{1}{ ilde c_{{m
ho}_\kappa}(h)}:=\sum_{j=0}^{d_{c_{{m
ho},\kappa}}}c_{\kappa,j}\left(rac{h}{10^6}
ight)^j.$$

Reconstruction of T

$$T(h,p_*) pprox ilde{T}(h) := egin{array}{c} ilde{T}_\ell(h) := T^s + \int_{h_\ell^s}^h rac{1}{ ilde{c}_{
ho_\ell}(h)} dh, & ext{if } h \leq h_\ell^s, \ T^s, & ext{if } h_\ell^s < h < h_g^s, \ ilde{T}_g(h) := T^s + \int_{h_g^s}^h rac{1}{ ilde{c}_{
ho_g}(h)} dh, & ext{if } h \geq h_g^s. \end{array}$$

For the quantities with low variations on the considered range for $h(\mu, \lambda, ...)$, we can use the same approach with d = 0.

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Influence of heating and choice of the model: steady solutions (monophasic ideal gas, no viscosity nor gravity, Φ , h_e , v_e constant)

• Compressible Euler without Φ

$$h^{\infty}=h_e, \qquad v^{\infty}=v_e$$

• Compressible Euler with Φ^{1}

$$\begin{cases} h^{\infty} = h_e \frac{2\gamma \tilde{p}_e + \gamma - 1 + \tilde{\Phi}y}{\gamma (\tilde{p}_e + 1) + \sqrt{(\gamma \tilde{p}_e + 1)^2 - (\gamma^2 - 1)\tilde{\Phi}y}},\\ v^{\infty} = \frac{v_e}{\gamma + 1} \left(\gamma (\tilde{p}_e + 1) - \sqrt{(\gamma \tilde{p}_e - 1)^2 - (\gamma^2 - 1)\tilde{\Phi}y}\right) \end{cases}$$

Low Mach model with Φ

$$h^{\infty} = h_e + rac{\Phi}{
ho_e v_e} y, \qquad v^{\infty} = v_e + rac{eta \Phi}{p_0} y$$

• Incompressible with Φ (Boussinesq approximation)

$$h^{\infty} = h_e + \frac{\Phi}{\rho_e v_e} y, \qquad v^{\infty} = v_e$$

$${}^{1}\tilde{\Phi} = 2\Phi/\rho_e v_e^3, \, \tilde{p}_0 = p_0/\rho_e v_e^2, \, \tilde{p}_e = \left(1 - \tilde{p}_0 + \sqrt{(\gamma \tilde{p}_0 - 1)^2 + \tilde{\Phi}L}\right)/(\gamma - 1).$$
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$$\begin{cases} \partial_{y} \mathbf{v} = \frac{\beta(h, p_{*})}{p_{*}} \Phi = -\frac{\rho'(h)}{\rho(h)^{2}} \Phi, \\ \rho(h)(\partial_{t} h + \mathbf{v} \partial_{y} h) = \Phi, \\ \rho(h)(\partial_{t} \mathbf{v} + \mathbf{v} \partial_{y} \mathbf{v}) + \partial_{y} \bar{p} = \partial_{y}(\mu \partial_{x} \mathbf{v}) - \rho(h)g. \end{cases}$$

Steady solution for any equation of state

• Observe that $\rho(h)v$ is constant (equal to D_e), thus $\left|v^{\infty}(y) = \frac{D_e}{\rho(h^{\infty}(y))}\right|$

Oeduce enthalpy:

$$h^\infty(y) = h_e + rac{\Psi(y)}{D_e}, \qquad ext{where } \Psi(y) := \int_0^y \Phi^\infty(z) \; \mathrm{d} z$$

Operation Operation Oper



Importance of approximating precisely the saturation values!

Exact solution with phase transition (NASG)

 Φ , v_e , h_e , h_0 : constants; IC and BC: liquid phase



Enthalpy: method of characteristics applied to $\partial_t h + v \partial_y h = \frac{\beta(h)\Phi}{p_*}(h - \hat{q}(h))$.

$$h(t,y) = \begin{cases} q_{\ell} + (h_0 - \hat{q}_{\ell})e^{\hat{\Phi}_{\ell}t} & \text{if } (t,y) \in \mathcal{L} \text{ and } t < t_{\ell}(y), \\ q_m + (h_{\ell}^s - \hat{q}_m)e^{\hat{\Phi}_m(t-t_{\ell}^s)} & \text{if } (t,y) \in \mathcal{M} \text{ and } t < t_m(y), \\ q_g + (h_g^s - \hat{q}_g)e^{\hat{\Phi}_g(t-t_g^s)} & \text{if } (t,y) \in \mathcal{G} \text{ and } t < t_g(y), \\ h_e + \frac{\Phi}{D_e}y & \text{else.} \end{cases}$$

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Higher dimensions: Weak formulation

Equivalent formulation when taking into account thermal diffusion

$$\begin{cases} \operatorname{div} \boldsymbol{u} = \frac{\beta(h)}{p_0} [\Phi + \operatorname{div}(\Lambda(h)\nabla h)] = \frac{\beta(h)\rho(h)}{p_0} [\partial_t h + \boldsymbol{u} \cdot \nabla h] \\ \rho(h) (\partial_t h + \boldsymbol{u} \cdot \nabla h) = \Phi + \operatorname{div}(\Lambda(h)\nabla h) \\ \rho(h) (\partial_t \boldsymbol{u} + (\boldsymbol{u} \cdot \nabla)\boldsymbol{u}) + \nabla \bar{p} = \operatorname{div}(\sigma(\boldsymbol{u})) + \rho(h)\boldsymbol{g} \end{cases}$$

- ► Allows to avoid boundary terms (after integration by parts) on $\{x \in \Omega : h(t, x) = h_{\kappa}^{s}\}$, thus avoid
 - to improve the regularity of the function space of p_{test}
 - to approximate $\frac{\partial \beta}{\partial h}$

and numerically, at each time step,

- to define the curves $h(t^n, \cdot) = h_{\kappa}^s$,
- to remesh to capture these zones.

Test case with localized heating and phase change

$D_e = 375 \, \mathrm{kg} \cdot \mathrm{m}^{-2} \cdot \mathrm{s}^{-1}, \; \rho_e = 750 \, \mathrm{kg} \cdot \mathrm{m}^{-3}, \; \Phi = 170 \times 10^6 \, \mathrm{W} \cdot \mathrm{m}^{-3} \mathbb{1}_D$



Influence of gravity

Enthalpy at time 0.55 s for several orientations of g (with phase change)



Rayleigh-Taylor instability / Gravity in competition with convection

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Conclusion and prospects

Conclusions

- Low Mach number model, fine treatment of the thermodynamics of phase change
- ► Easier for mathematical analysis (steady and exact solutions)
- Easier for numerical simulations

Work in progress and prospects

- Analysis of the mode without thermal diffusion (boundary conditions)
- Analysis of the model with thermal diffusion (discontinuity of Λ)
- Deriving a hierarchy of models (relaxation of the different equilibria, cf. *n*-equations models in the compressible setting)
 - \rightarrow convergences between the different models
- \blacktriangleright Coupling with simplified neutronics equations to determine Φ

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Thank you for your attention!

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Low Mach number models

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